

ENGINEERING AND COMPLIANCE DIVISION

APPLICATION PROCESSING AND CALCULATIONS

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PERMIT TO CONSTRUCT ANALYSIS

COMPANY NAME

Eastern Municipal Water District
San Jacinto
Reclamation Facility

AEIS NUMBERS:

19159

PERMITEE/OPERATOR

SAME AS FORM 400A

EQUIPMENT LOCATION

SAME AS FORM 400A

Applications(s):

See Below

EQUIPMENT DESCRIPTION

APPLICATION NO. 473572 [PREVIOUS APPL.NO.448181, PO F83291]
[TO BE CANCELLED SUPERSEDED BY APPLICATION NO. 475846]

APPLICATION NO. 475846 [PREVIOUS APPL.NO.448181, PO F83291]

MODIFICATION OF A WATER RECLAMATION PLANT, ANAEROBIC, 11 MGD CAPACITY:

I. HEADWORKS PROCESSES CONSISTING OF:

1. ONE (1) CLIMBING BAR SCREEN WITH RAG COMPACTOR AND ONE (1) COMMINUTOR FOR BACKUP.
2. ONE (1) STORAGE TANK, FERRIC CHLORIDE, 2,500 GALS.
3. THREE (3) AERATED GRIT CHAMBERS WITH ASSOCIATED PUMPS AND MOTORS.
4. ONE (1) GRIT WASHER AND HOPPER WITH ASSOCIATED PUMPS AND MOTORS.

II. PRIMARY TREATMENT PROCESSES CONSISTING OF:

5. FIVE (5) PRIMARY SEDIMENTATION TANKS, UNCOVERED, EACH 16' W X 123' L X 12' H, WITH ASSOCIATED DRIVES, PUMPS AND MOTORS.
6. FIVE (5) AERATION TANKS, EACH 24' W X 210' L X 15' H, WITH ASSOCIATED PUMPS AND MOTORS.

III SECONDARY TREATMENT PROCESSES CONSISTING OF:

7. ELEVEN (11) SECONDARY SEDIMENTATION TANKS, EACH 16' W X 110' L X 12' H, WITH ASSOCIATED PUMPS AND MOTORS.
8. TWO (2) FLOW EQUALIZATION BASINS, EACH 2.5 MILLION GALLONS PER DAY CAPACITY, 150' W X 420' L X 3' H, WITH ASSOCIATED PUMPS AND MOTORS.
9. TWO (2) STORAGE TANKS, CHLORINE, 10 TON CAPACITY, EACH 4'-6" D X 16'-11" L.
10. SCRUBBER, CHLORINE NEUTRALIZING, RJ-2000 BULK.
11. ONE (1) STORAGE TANK, CAUSTIC SODA, 14,500 GALLON CAPACITY, 16' D X 10' H.

Appl. No: 473572, 475844, 475845, and 475846

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12. TWO (2) CHLORINE CONTACT TANKS, EACH 28'-6" W X 235' L X 12' H.
 13. TEN (10) SECONDARY EFFLUENT EVAPORATION/STORAGE PONDS, 264 MILLION GALLONS TOTAL CAPACITY.
 14. TWELVE (12) WETLAND RESEARCH CELLS, EACH 45' W X 225' L X 2' H.
 15. ONE (1) CONSTRUCTED WETLANDS, 40 MILLION GALLON CAPACITY, 25 ACRES, 5' DEEP.

IV. SLUDGE PROCESSES CONSISTING OF:

16. TWO (2) DISSOLVED AIR FLOATION (DAF) SLUDGE THICKENER TANKS, EACH 30' D X 6' H, WITH ASSOCIATED PUMPS AND MOTORS.
17. THREE (3) PRIMARY DIGESTERS WITH FIXED ROOF, EACH 50' D X 22' H, EACH 309,000 GALLONS, WITH ASSOCIATED PUMPS AND MOTORS.
19. ONE (1) GAS DRYER WITH ASSOCIATED MOTOR.
20. ONE (1) DIGESTER GAS STORAGE SPHERE, 35' D, WITH GAS COMPRESSOR.
21. ONE (1) DIGESTER GAS DESULFURIZATION (IRON SPONGE), GROTH EQUIPMENT CORPORATION, DUAL VESSEL, EACH VESSEL, 5' W X 9'-9" L X 7'-1" H, EACH CELL CONTAINING 112 CUBIC FEET OF FERRIC OXIDE MATERIAL.
22. ONE (1) SLUDGE OFF-LOADING STATION.
23. TWO (2) SLUDGE DRYING BEDS, EACH 160' W X 140' L X 1' H.
24. EIGHT (8) SLUDGE DRYING BEDS, EACH 40' W X 140' L X 1' H.
25. ONE (1) STORAGE TANK, CAUSTIC SODA, 1,000 GALLONS.
26. TWO (2) BOILERS, FULTON PULSEPAK, MODEL PHW 1400, 1.4 MMBTU/HR EACH, NATURAL GAS FIRED.
27. ONE (1) SCRUBBER, WESTERN TECHNOLOGY, PACKED BED, 8' D X 16'-8" H.
28. PASTEURIZATION SYSTEM, FULLY ENCLOSED TO THE ATMOSPHERE, ECO-THERM, WITH A VARIABLE SPEED FEED PUMP, SPIRAL-TYPE HEAT EXCHANGERS AND TWO SERPENTINE PIPE REACTORS.

V. TERTIARY TREATMENT PROCESSES, 22 MGD CAPACITY, CONSISTING OF:

29. FOUR TERTIARY FILTERS, ROTARY DISC CLOTH TYPE, EACH 636 SQUARE FEET.

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BY THE ADDITION OF:

I. HEADWORKS:

1. TWO BAR SCREENS, WITH SCREW CONVEYOR, WASHER, COMPACTOR, AND BIN
2. TWO GRIT BASINS, CIRCULAR VORTEX TYPE, 18'-0" DIA.
3. SPLITTER BOX, WITH ASSOCIATED DRIVES, PUMPS AND MOTORS.

II. PRIMARY TREATMENT:

4. TWO STORAGE TANKS, FERRIC CHLORIDE, EACH 11,000 GALLONS CAPACITY,
5. FIVE PRIMARY CLARIFIERS, COVERED, EACH 16' W. X 123' L. X 12' H. WITH ASSOCIATED DRIVES, PUMPS AND MOTORS.
6. INFLUENT SPLITTER BOX, WITH ASSOCIATED DRIVES, PUMPS AND
7. TWO PRIMARY CLARIFIERS, COVERED, EACH 100'-0" DIA. X 12'-0" D., WITH ASSOCIATED DRIVES, PUMPS AND MOTORS. (PLANT 2)
8. PRIMARY EFFLUENT SPLITTER BOX, WITH ASSOCIATED DRIVES, PUMPS AND MOTORS. (PLANT 2)

III. SECONDARY TREATMENT

9. AERATION TANK, 160' W X 200' L X 15' H, WITH ASSOCIATED PUMPS AND MOTORS. (Plant 2)
10. THREE SECONDARY CLARIFIERS, EACH 125' DIA X 14' H, WITH ASSOCIATED DRIVES, PUMPS AND MOTORS. (PLANT 2)
11. ONE CHLORINE CONTACT TANK, 28'-6" W X 235' L X 12' H.
12. FLOW EQUALIZATION BASIN, NO.1 (NORTH), 452' L. X 138' W. X 5' D., 2.5 MILLION GALLONS CAPACITY.
13. FLOW EQUALIZATION BASIN, NO.2 (SOUTH), 452' L. X 160' W. X 5' D., 2.5 MILLION GALLONS CAPACITY.
14. FOUR SECONDARY EFFLUENT AND SIX TERTIARY EFFLUENT STORAGE PONDS, 264 MILLION GALLONS TOTAL CAPACITY.

IV. SLUDGE PROCESSES

15. SCUM DECANT STATION
16. THREE ROTARY DRUM THICKENERS, WITH ASSOCIATED PUMPS AND POLYMER BLENDING UNITS
17. TWO PRIMARY DIGESTERS, DOMED ROOF, 80'-0" DIA. X 42'-0" H., EACH 1,127,958 GALLONS CAPACITY, WITH ASSOCIATED PUMPS, MOTORS, AND HEATING EQUIPMENT
18. ONE (1) STORAGE TANK, COLD SLUDGE, WITH FIXED DOMED COVER, SECONDARY DIGESTER WITH FLOATING ROOF, 50' D X 22' H, 293,005 GALLONS.
19. ONE STORAGE TANK, DIGESTED SLUDGE, 80'-0" DIA. X 23'-0" H., 864,767 GALLONS CAPACITY.
20. ONE PRE-HEAT TANK (EXISTING BUT NOT LISTED)
21. ONE STORAGE TANK, DIGESTER GAS (LOW PRESSURE), 24' D X 30'-0" H.
22. THREE CONVEYORS, SLUDGE CAKE,

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23. PASTEURIZATION SYSTEM, WITH VARIABLE SPEED FEED PUMP, SPIRAL-TYPE HEAT EXCHANGERS, TWO SERPENTINE PIPE REACTORS, AND CARBON ADSORBER.
24. TWO DIGESTER GAS DESULFURIZATION TANKS, IRON SPONGE, VAREC MODEL VB2350800, EACH 9'-11' L. X 5'-7" W. X 6'-3" H.
25. SLUDGE DRYING BEDS,
 - A. TWO BEDS, 160' W. X 140' L. X 1' D.
 - B. TWO BEDS, 40' W. X 140' L. X 1' D.
 - C. TWO BEDS, 120' W. X 140' L. X 1' D.

V. TERTIARY TREATMENT PROCESSES:

26. SECONDARY EFFLUENT EQUALIZATION BASIN, NO.1, 138'-0" W. X 452'-0" L. X 4'-0" H., 2.0 MILLION GALLONS CAPACITY
 27. SECONDARY EFFLUENT EQUALIZATION BASIN, NO.2, 160'-0" W. X 452'-0" L. X 4'-0" H., 2.3 MILLION GALLONS CAPACITY
 28. TWO FLOCCULATION BASINS, EACH 18'-0" L. X 18'-0" W. X 20'-0" H., WITH ALUM AND POLYMER STORAGE, PUMPING EQUIPMENT, TWO RAPID MIX BOXES, FOUR FLOCCULATORS, AND ASSOCIATED PUMPS AND MOTORS.
 29. TWO TERTIARY FILTERS, ROTARY DISC CLOTH TYPE, EACH 636 SQUARE FEET.
 30. TERTIARY EFFLUENT DIVERSION BOX
 31. SEVEN STORAGE PONDS, TREATED EFFLUENT, 223.6 MILLION GALLONS CAPACITY
 32. THREE STORAGE PONDS, OUT-OF-COMPLIANCE EFFLUENT, 34.2 MILLION GALLONS CAPACITY
 33. STORAGE TANK, ALUM/POLYMER, 10' DIA. X 12' H.
- AND THE REMOVAL OF:

I. HEADWORKS:

1. ONE (1) CLIMBING BAR SCREEN WITH RAG COMPACTOR AND ONE (1) COMMUNUTOR FOR BACKUP.
2. ONE (1) STORAGE TANK, FERRIC CHLORIDE, 2,500 GALS.
3. THREE (3) AERATED GRIT CHAMBERS WITH ASSOCIATED PUMPS AND MOTORS.
4. ONE (1) GRIT WASHER AND HOPPER WITH ASSOCIATED PUMPS AND MOTORS.

II. PRIMARY TREATMENT:

5. FIVE PRIMARY SEDIMENTATION TANKS, COVERED, EACH 16' W X 123' L. X 12' H., WITH ASSOCIATED DRIVES, PUMPS AND MOTORS.

III. SECONDARY TREATMENT

6. TEN SECONDARY EFFLUENT EVAPORATION/STORAGE PONDS, 264 MILLION GALLONS TOTAL CAPACITY.

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IV. SLUDGE PROCESSES

7. TWO DISSOLVED AIR FLOATATION (DAF) SLUDGE THICKENER TANKS, EACH 30'-0" DIA. X 6'-0" H. WITH ASSOCIATED PUMPS AND MOTORS.
8. ONE (1) SECONDARY DIGESTER WITH FLOATING ROOF, 50' D X 22' H, 293,005 GALLONS.
9. EIGHT (8) SLUDGE DRYING BEDS, EACH 40' W X 140' L X 1' H.
10. ONE (1) STORAGE TANK, CAUSTIC SODA, 1,000 GALLONS.
11. ONE (1) SCRUBBER, WESTERN TECHNOLOGY, PACKED BED, 8' D X 16'-8" H.
12. PASTEURIZATION SYSTEM, FULLY ENCLOSED TO THE ATMOSPHERE, ECO-THERM, WITH A VARIABLE SPEED FEED PUMP, SPIRAL-TYPE HEAT EXCHANGERS TWO SERPENTINE PIPE REACTORS.
13. ONE (1) DIGESTER GAS DESULFURIZATION (IRON SPONGE), GROTH EQUIPMENT CORPORATION, DUAL VESSEL, EACH VESSEL, 5' W X 9'-9" L X 7'-1" H, EACH CELL CONTAINING 112 CUBIC FEET OF FERRIC OXIDE MATERIAL.

TERTIARY TREATMENT PROCESSES:

14. TWO (2) FLOW EQUALIZATION BASINS, EACH 2.5 MILLION GALLONS PER DAY CAPACITY, 150' W X 420' L X 3' H, WITH ASSOCIATED PUMPS AND MOTORS.

AND BY INCREASING THE PLANTS TREATING CAPACITY FROM 11 MGD TO 14 MGD

CONDITIONS: (See Sample permit)

APPLICATION NO. 471708

AIR POLLUTION CONTROL SYSTEM CONSISTING OF:

1. BIOFILTER, CUSTOM, TWO CELLS OPERATING IN PARALLEL, EACH CELL 75'-0" W X 75'-0" L.
2. TWO BLOWERS, EACH 15,000 CFM
3. EXHAUST SYSTEM, 30,000 CFM MAXIMUM CAPACITY, VENTING THE WET WELL, HEADWORKS, GRIT CHAMBER, AND PRIMARY CLARIFIERS.

CONDITIONS: (See Sample permit)

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BACKGROUND

The Eastern Municipal Water District (EMWD), ID No. 19159, filed application No. 473572, on September 13, 2007 and applications No. 475845, 475846, and 475844, on November 27, 2007. Application No. 473572 will be cancelled because it was superseded by application No. 475846. Application No. 475846 was filed to modify the waste water treatment plant subject to permit to operate No. F83291 (Appl.No.448181) which was issued in February 1, 2007. The waste water treatment plant capacity will be increased to 14 MGD from 11 MGD. Application No. 475845 was filed to construct a new biofilter which will vent the headworks and primary clarifiers in the plant expansion. Application No. 475844 was filed for a Deminimus Significant Revision to the initial Title V Facility Permit issued on February 1, 2007.

A Notice of Determination was recorded on April 4, 2007, for an approved negative declaration (CEQA Document) for this project.

PROCESS DESCRIPTION

The San Jacinto Valley Regional Water Reclamation Facility (SJVRRWF) services a 167 square mile service area, which includes the cities of Hemet and San Jacinto. The current capacity of the waste water treatment system is 11 MGD, and operating schedule is 24 hr/day, 365 days per week.

The EMWD is proposing to increase the capacity of the facility to 14 MGD by installing new equipment and modifying or removing the existing equipment. The existing head works will be demolished and replaced with new equipment, the effluent will be split into two parallel trains consisting of primary and secondary treatment plants (No.1, and No.2). To increase the capacity of the Headworks, two new bar screens, two vortex type grit chambers will be installed and then the existing bar screen, and grit chamber will be removed. A splitter box will be used to direct the flow to two separate primary treatment trains.

The new clarifiers (plant No.2) will be installed to provide the full capacity of the 14 MGD gallon expansion and will be covered with a dome and vented to the new biofilter, while the existing primary clarifiers (in plant 1) will be used as standby equipment to supplement the new equipment during wet season operation. A splitter box will direct the effluent to two secondary treatment trains.

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The existing primary treatment process (plant No.1) consists of five aeration basins, eleven secondary sedimentation tanks, twelve wetland research cells, and 25 acre wetlands area. These areas will be receive minor piping modifications. Three new clarifiers and a new aeration basin comprise plant No.2. The secondary effluent flows into two flow equalization basins which will be modified slightly to allow the construction of two new flocculation basins. The ten secondary effluent evaporation ponds will be split into two groups used for either secondary effluent or tertiary effluent storage ponds. The total capacity will remain the same at 264 million gallons. The two existing chlorine contact basins will be supplemented by the addition of a third chlorine contact basin.

The tertiary treatment plant will be upgraded by installing two new rotary filters to increase the capacity required to process the secondary effluent from plants No.1 and No.2. These filters are identical to the existing filters. The tertiary filters are also chlorinated to prevent bacterial growth in the filters. The existing storage ponds will be modified to provide tertiary effluent storage with a total capacity of 223.6 million gallons. The ponds are also modified to provide 34.2 million gallons storage for out-of -compliance effluent.

The Sludge treatment plant will be upgraded also to increase the capacity of the system and process the solids from both plants No. 1, and No. 2. The sludge treatment plant will be modified by removing the DAF units and then replacing the equipment with a new scum decant station, and three rotary drum thickeners to process the WAF from each plant. The pasteurizer was modified by passively venting it to a carbon adsorber for odor control.

To increase the capacity of the existing primary anaerobic digesters, two new primary digesters will be added to supplement the existing digesters. The existing secondary digester will be converted to a cold sludge storage tank and the floating dome cover will be replaced with a fixed cover. The digester gas will be collected in a new low pressure gas storage tank which will feed the existing high pressure digester gas storage sphere. The digester gas will be treated with two adsorbers which are both filled with iron sponge media to remove the H₂S. The treated gas is burned in the existing engines, boiler or flare. The existing unit was replaced and a second additional iron sponge vessel was added for redundancy.

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The sludge from the digesters is processed in the existing centrifuge, and belt press system in the dewatering building. The filter cake from the belt press system is conveyed to a hopper/truck loading station, or sent to the sludge drying beds. The eight sludge drying beds will be redivided into six beds with the same surface area and capacity of the original beds.

The new biofilter will vent the headworks building, grit chamber, and new primary clarifiers for odor control.

See Appendix F for a process flow diagram.

EMISSIONS

The VOC emissions from the existing and proposed and existing waste water treatment system were estimated in appendix B using the JEIP factors. H2S emissions from the biofilter were estimated in Appendix C based on a permit limit of 1 ppmv, and a outlet flow rate of 30,000 cfm. The VOC, and H2S emissions are estimated as follows:

	VOC			H2S			
	Appl.No.	lb/hr	lb/day	lb/year	lb/hr	lb/day	lb/year
Uncont.	475846	1.95	46.7	17063	1.08	25.8	9424
Cont.	475846	1.95	46.7	17063	0.16	3.9	1414
Uncont.	448181	1.59	38.2	13955	--	--	--
Cont.	448181	1.59	38.2	13955	--	--	--
	Increase	0.35	8.5	3108	1.08	25.8	9424

The Ammonia emissions from the existing and proposed and existing waste water treatment system were estimated in appendix D using the Lake Michigan Air Directors Consortium emission factor.

Ammonia Emissions				
	Appl.No.	lb/hr	lb/day	lb/year
Uncont.	475845	0.07	1.7	612
Cont.	475845	0.07	1.7	612
Uncont.	448181	0.06	1.3	480
Cont.	448181	0.06	1.3	480
	Increase	0.02	0.4	131

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EVALUATION

Rule 212

Rule 212(c)(2)- The emissions increase due to this modification does not exceed the limits specified in subdivision (g) of this Rule. Furthermore, the MICR will be less than 1 in a million, and there is no school located within 1000 feet of this facility. No public notice is required and the proposed project complies with Rule 212.

Rule 401

No visible emissions are expected from the normal operation of this equipment. Therefore compliance with Rule 401 is expected.

Rule 402

The headworks, grit chambers, primary influent splitter box, primary clarifiers, primary scum pit, primary effluent splitter box, and sludge dewatering building are vented to air pollution controls.

The concentration of H₂S is estimated (in Appendix D) at 7.0 PPBV at 200 meters at the closest receptor from the biofilter exhaust.

Therefore, the maximum ground level concentrations for H₂S are much less than 30 ppbv which is the California State Ambient Air Quality Standard at the facility property boundary. This standard was adopted to protect against nuisance odor for the general public. The maximum concentration of H₂S is also less than 8 ppbv odor threshold level listed by California Office of Environmental Health Hazard Assessment Office (OEHHA) which can be detected but unlikely to be recognized or found annoying by more than a few people. Therefore, all equipment is expected to comply with Rule 402.

Rule 431.1

The biogas generated by the digesters, is vented through a adsorber to removed H₂S, and the maximum concentration is limited to less than 200 ppmv by a permit condition which existing on the original permit to construct issued under application No. 117529 in 1988. Furthermore, the facility is subject to a facility condition limiting the SO_x emissions to 5 lb/day. Therefore, compliance with Rule 431.1 is expected.

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Rule 1303 - BACT & Offsets

Since the headworks, and primary clarifiers are vented to a biofilter and the digester gas is vented to a collection system, the proposed construction complies with BACT for VOC. Sox emissions are controlled with a ferric chloride adsorption system (Iron Sponge) to limit the emissions of H2S and to comply with BACT. Therefore, compliance with Rule 1303 is expected.

Rule 1401

Based on the permit conditions for the Biofilter limiting H2S emission to less than 1 ppmv, a Tier II risk assessment the HI is less than 1. Furthermore, based on the BASTE model by the applicant the risk from the Waste water treatment system is estimated at 0.31 in a million, and HI is estimated at 0.22 based on a Tier II risk assessment. Therefore, compliance with Rule 1401 risk assessment is expected.

Rule 1401.1

Since this facility was constructed under AQMD permits which were issued prior to November 4, 2005, this is an existing facility as defined in section (c)(3)(A), which is exempt from Rule 1401.1

Rule 3004

A De minimis Significant Permit Revision can be recommended under Application No. 475844, because the equipment proposed under Applications No.475845, and 475846, meet the criteria listed in Table 3-8, De Minimis Significant Permit Revision Criteria, in the Technical Guidance Document for Title V dated January 1998.

There is no CAM Plan requirement because there is no applicable emission limit or standard, this is not a large source, and the initial Title V permit was filed before April 1998. The existing conditions in the Title V facility permit in Sections D, E, and K, are sufficient to assure compliance with the monitoring, recordkeeping, and reporting required by Title V.

Since the Facility has certified compliance with all Rules and Regulations, and there is no recent NOV or NOC issued by the AQMD, a de minimis significant revision to the Title V Facility Permit, can be recommended subject to EPA Review.

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RECOMMENDATION

Since the proposed expansion of the waste-water treatment plant is constructed using BACT, and no nuisance is expected, application No. 475846, is expected to comply with all AQMD Rules and Regulations. Furthermore, the Biofilter subject to application no 475845, is used for odor control to comply with Rule 402. Therefore, Application numbers 475846, and 475845, are recommended for permit to construct with the proposed equipment and descriptions, and application No. 473572 is recommended for cancellation. Consequently, a De minimus Significant Revision to the initial Title V facility permit issued on February 1, 2007, is recommended.