

**PERMIT APPLICATION REVIEW
COVERED SOURCE PERMIT NO. 0081-01-C
Renewal Application No. 0081-04**

Applicant: Chevron Products Company
Facility: Kahului Marketing Terminal
Location: 100-A Hobron Avenue, Kahului, Maui

**Mailing
Address:** 100-A Hobron Avenue
Kahului, Hawaii 96732

Coordinates: UTM: 764,697 meters East and 2,312,892 meters North (NAD 83)

- Equipment:**
- a. 7,130 barrel internal floating roof storage tank with mechanical shoe primary seal and single wiper secondary seal, Tank No. 1;
 - b. 1,537 barrel internal floating roof storage tank with mechanical shoe primary seal and single wiper secondary seal, Tank No. 2;
 - c. 1,258 barrel internal floating roof storage tank with mechanical shoe primary seal and single wiper secondary seal, Tank No. 7;
 - d. 1,105 barrel internal floating roof storage tank with mechanical shoe primary seal and single wiper secondary seal, Tank No. 9;
 - e. 9,398 barrel internal floating roof storage tank with mechanical shoe primary seal and single wiper secondary seal, Tank No. 11;
 - f. 3,779 barrel internal floating roof storage tank with mechanical shoe primary seal and single wiper secondary seal, Tank No. 13;
 - g. Transmix storage tank(s);
 - h. Bottom loading load rack with two (2) loading lanes and six (6) product load arms per loading land; and
 - i. 4,800 gallon/minute capacity John Zink vapor combustion system, model no. ZCT-2-8-35-X-2/8-X-X, serial no. VC-954537.

Responsible

Official: Hugh Meshell
Title: Terminal Manager
Phone: (808) 877-5012
Cell: (808) 357-1041
Address: 100-A Hobron Avenue
Kahului, Hawaii 96732

Contact: Todd E. Osterberg
Title: HES Specialist - Logistics
Phone: (808) 527-2747
Address: 777 North Nimitz Highway
Honolulu, Hawaii 96817

1. Background.

1.1 Chevron Products Company has submitted a renewal application for its covered source permit to operate Kahului Marketing Terminal. The terminal uses a bottom loading load rack to distribute products that include motor gasoline, diesel fuel, ethanol, naphtha (straight run gasoline), and jet fuel. The load rack is equipped with a vapor combustion system to control volatile organic compounds (VOCs). The total combined throughput of the load rack is limited to 5,631,429 barrels per year of aviation gasoline, denatured ethanol, motor gasoline, and naphtha (whole straight run gasoline). Product is received primarily from the Chevron Honolulu Marine Terminal on Oahu via barges and is stored at the terminal in above ground storage tanks. The Kahului Marketing Terminal occasionally

obtains product from other sources. The standard industrial classification code for this facility is 5171 (Petroleum Bulk Stations and Terminals).

1.2 The applicant disclosed the following information:

- a. The average gasoline throughput for the terminal was 73,909 gallons per day in 2008 and 68,892 gallons per day in 2009.
- b. No decision has been made on how to comply with the new federal regulations that specify requirements for transmix storage. The vapor combustion system servicing the load rack may be used to control VOCs, however, other options may be considered.

2. Applicable Requirements

2.1 Hawaii Administrative Rules (HAR)

Chapter 11-59, Ambient Air Quality Standards

Chapter 11-60.1, Air Pollution Control

Subchapter 1, General Requirements

Subchapter 2, General Prohibitions

§11-60.1-31 Applicability

§11-60.1-31 Storage of Volatile Organic Compounds

§11-60.1-41 Pump and Compressor Requirements

Subchapter 5, Covered Sources

Subchapter 6, Fees for Covered Sources, Noncovered Sources, and
Agricultural Burning

§11-60.1-111 Definitions

§11-60.1-112 General Fee Provisions for Covered Sources

§11-60.1-113 Application Fees for Covered Sources

§11-60.1-114 Annual Fees for Covered Sources

§11-60.1-115 Basis of Annual Fees for Covered Sources

Subchapter 8, New Source Performance Standards

§11-60.1-161 New Source Performance Standards

2.2 40 Code of Federal Regulations (CFR), Part 60 – New Source Performance Standards (NSPS), Subpart K, Standards of Performance for Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After June 11, 1973 and Prior to May 19, 1978 is not applicable to the gasoline storage tanks.

2.3 40 CFR, Part 60 – NSPS, Subpart Ka, Standards of Performance for Storage Vessels for Petroleum Liquids for Which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984 is not applicable to the gasoline storage tanks.

2.4 40 CFR, Part 60 – NSPS, Subpart Kb, Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for which Construction, Reconstruction, or Modification Commenced after July 23, 1984 is not applicable to gasoline storage tanks because tanks at this facility were not constructed, reconstructed, or modified after 1984.

2.5 40 CFR, Part 60 – NSPS, Subpart XX, Standards of Performance for Bulk Gasoline Terminals is applicable to the bottom loading load rack because the load rack was constructed after December 17, 1980.

- 2.6 40 CFR Part 63, Subpart BBBBBB – National Emission Standards for Hazardous Air Pollutants for Source Category: Gasoline Distribution Bulk Terminals, Bulk Plants, and Pipeline Facilities is applicable because this facility emits hazardous air pollutants (HAPs) from an area source gasoline distribution bulk terminal. The facility is designated a gasoline distribution bulk terminal because the gasoline throughput, based on the facility's permit limit, is greater than 20,000 gallons per day. Option 2 from Table 2 of 40 CFR Part 63, Subpart BBBBBB, applies to the load rack because records indicate the actual gasoline throughput is less than 250,000 gallons per day. Tank Nos. 1, 2, 7, 9, 11, 13, and 14 are subject to 40 CFR Part 63, Subpart BBBBBB, because the tanks are located at a gasoline distribution bulk terminal and store gasoline.
- 2.7 The Consolidated Emissions Reporting Rule (CERR) is not applicable because emissions from the facility do not exceed reporting levels pursuant to 40 CFR 51.
- 2.8 A best available control technology analysis (BACT) analysis is required for new sources or modifications to existing sources that would result in a significant emissions increase as defined in HAR, Section 11-60.1. There are no modifications at the terminal that increase emissions above significant emission thresholds. As such, BACT is not applicable.
- 2.9 The purpose of Compliance Assurance Monitoring (CAM) is to provide reasonable assurance that compliance is being achieved with large emissions units that rely on air pollution control device equipment to meet an emissions limit or standard. Pursuant to 40 CFR, Part 64, for CAM to be applicable, the emissions unit must: (1) be located at a major source; (2) be subject to an emissions limit or standard; (3) use a control device to achieve compliance; (4) have potential pre-control emissions that are greater than the major source level; and (5) not otherwise be exempt from CAM. Although the load rack relies on a vapor combustion system to achieve compliance with the VOC standards (e.g., standard for load racks specified in 40 CFR Part 60, Subpart XX and standard for closed vent systems with control devices specified in 40 CFR Part 63, Subpart BBBBBB), and has potential pre-control emissions greater than the major source level for VOCs, CAM is not applicable because this facility is not a major source.
- 2.10 Prevention of significant deterioration (PSD) does not apply because emissions from the terminal are less than major source thresholds.
- 2.11 The facility is a synthetic minor source because the throughput limitation of 5,631,429 barrels (236,520,018 gallons) per year ensures that emissions from the facility are below major source thresholds. Maximum capacity of the terminal is 4,800 gallons per minute or 2,522,880,000 gallons per year based on the vapor combustion system's capacity.

3. Insignificant Activities

- 3.1 The following is a list of insignificant activities at the marketing terminal. Tanks listed in (a) through (e), (g), (h), (j), and (k) are exempt pursuant to HAR §11-60.1-82(f)(7). Tanks listed in (i) and (l) are exempt in accordance with HAR §11-60.1-82(f)(1). The sump and oil water separator listed in (m) and (n) are exempt pursuant to HAR §11-60.1-82(f)(7).
- a. 18,497 barrel vertical fixed roof Tank No. 3 storing low sulfur diesel;
 - b. 5,011 barrel vertical fixed cone roof Tank No. 4 storing Jet-A;
 - c. 3,546 barrel vertical fixed cone roof Tank No. 5 storing ultra-low-sulfur diesel;
 - d. 1,489 barrel vertical fixed cone roof Tank No. 6 storing Jet-A;
 - e. 5,859 barrel vertical fixed cone roof Tank No. 10 storing Jet-A;
 - f. 546 barrel vertical fixed cone roof Tank No. 14 storing transmix, except when subject to 40 CFR Part 63, Subpart BBBB;B;
 - g. 11,078 barrel vertical fixed cone roof Tank No. 15 that is out of service;
 - h. 1,470 barrel vertical fixed cone roof Tank No. 19 storing ultra-low-sulfur diesel;
 - i. 929 barrel vertical fixed cone roof Tank No. 20 that is out of service;
 - j. 7,724 gallon horizontal fixed roof additive Tank No. 22;
 - k. 7,724 gallon horizontal fixed roof additive Tank No. 23;
 - l. 499 gallon propane tank;
 - m. 9,800 gallon concrete sump; and
 - n. 350 gallon oil water separator.

4. Alternate Operating Scenarios

- 4.1 No alternate operating scenarios were proposed for the permit renewal.

5. Project Emissions

- 5.1 Potential emissions from the bottom loading load rack with vapor combustion system were based on the following:
- a. Maximum permitted throughput of 5,631,429 barrels/year (236,520,018 gallons/year);
 - b. Maximum 4,800 gallon/minute gasoline throughput and manufacturer's data to determine NO_x and CO emissions;
 - c. Loading of gasoline into cargo tanks as worst-case scenario;
 - d. Maximum VOC emission of 35 mg per liter of gasoline loaded based on standard specified for total organic compounds (TOCs) in 40 CFR;
 - e. A VOC emission factor of 8 mg/liter for leakage from cargo tanks when loading gasoline based on a November 7, 2001 memo regarding EPA Emission Factors for Tank Truck Loading;
 - f. An emission factor for NO_x of 4 mg/liter of gasoline loaded based on manufacturer's information;
 - g. An emission factor for CO of 10 mg/liter of gasoline loaded based on manufacturer's information;
 - h. Use of a mass balance calculation to determine SO₂ emissions (it was assumed that 0.1% sulfur was present in VOCs from tank truck loading losses). Available literature indicates that gasoline contains as much as 1,000 ppm sulfur (0.1% sulfur). The AP-42 emission factor (12.46 SPM/T) was used to determine loading losses. A saturation factor (S) of 0.6 for bottom loading tank truck – normal dedicated service was used. The true vapor pressure (P) was assumed to be 11 psia. The molecular weight (M) of

gasoline was assumed to be 66. A temperature (T) of 536 °R (76 °F + 460) was used for the equation);

- i. Use of vapor mass fractions for components from gasoline multiplied by the total VOC emissions to determine HAP emissions; and
- j. Potential emissions are summarized as follows:

Bottom Loading Load Rack (Gasoline)				
Pollutant	Vapor Mass Fraction	Emission (lb/hr)	Emission (g/s)	Emission (TPY)
VOC (see Notes a & b)	-----	-----	-----	42.5
NO _x (see Notes c, d, & e)	-----	9.620	1.215	4.0
CO (See Notes f, g, & h)	-----	24.050	3.037	9.9
SO _x (See Notes i, j, k, & l)	-----	5.813	0.734	2.4
Benzene	0.0060	-----	-----	0.255
Hexane (n)	0.0053	-----	-----	0.225
Toluene	0.0072	-----	-----	0.306
Xylene (-m)	0.0022	-----	-----	0.094
Total HAPs----->				0.880

- a: $(35 \text{ mg VOC/liter})(236,520,018 \text{ gal/yr})(\text{liter}/0.264 \text{ gal})(10^{-3} \text{ g/mg})(\text{kg}/1,000 \text{ g})(2.2046 \text{ lb/kg})(\text{ton}/2,000 \text{ lb}) = 34.565 \text{ TPY VOC from vapor combustion system}$
- b: $(8 \text{ mg VOC/liter})(236,520,018 \text{ gal/yr})(\text{liter}/0.264 \text{ gal})(10^{-3} \text{ g/mg})(\text{kg}/1,000 \text{ g})(2.2046 \text{ lb/kg})(\text{ton}/2,000 \text{ lb}) = 7.900 \text{ TPY VOC from tank truck cargo tank leaks}$
- c: $(4,800 \text{ gal/min})(4 \text{ mg NO}_x/\text{liter})(\text{liter}/0.264 \text{ gal})(10^{-3} \text{ g/mg})(\text{kg}/1,000 \text{ g})(2.2046 \text{ lb/kg})(60 \text{ min/hr}) = 9.620 \text{ lb/hr NO}_x$
- d: $(9.620 \text{ lb NO}_x/\text{hr})(\text{hr}/3,600 \text{ sec})(\text{kg}/2.2 \text{ lb})(1,000 \text{ g/kg}) = 1.215 \text{ g/sec NO}_x$
- e: $(4 \text{ mg NO}_x/\text{liter})(236,520,018 \text{ gal/yr})(\text{liter}/0.264 \text{ gal})(10^{-3} \text{ g/mg})(\text{kg}/1,000 \text{ g})(2.2046 \text{ lb/kg})(\text{ton}/2,000 \text{ lb}) = 3.950 \text{ TPY NO}_x$
- f: $(4,800 \text{ gal/min})(10 \text{ mg CO/liter})(\text{liter}/0.264 \text{ gal})(10^{-3} \text{ g/mg})(\text{kg}/1,000 \text{ g})(2.2046 \text{ lb/kg})(60 \text{ min/hr}) = 24.050 \text{ lb/hr CO}$
- g: $(24.050 \text{ lb CO/hr})(\text{hr}/3,600 \text{ sec})(\text{kg}/2.2 \text{ lb})(1,000 \text{ g/kg}) = 3.037 \text{ g/sec CO}$
- h: $(10 \text{ mg CO/liter})(236,520,018 \text{ gal/yr})(\text{liter}/0.264 \text{ gal})(10^{-3} \text{ g/mg})(\text{kg}/1,000 \text{ g})(2.2046 \text{ lb/kg})(\text{ton}/2,000 \text{ lb}) = 9.876 \text{ TPY CO}$
- i: $12.46(0.6)(11)(66)/536 (0.1/100) = 0.0101 \text{ lb sulfur}/1,000 \text{ gal} = 0.0101(64.06/32.06 \text{ S}) = 0.0202 \text{ lb SO}_2/1,000 \text{ gal}$
- j: $(0.0202 \text{ lb SO}_2/1,000 \text{ gal})(4,800 \text{ gal/min})(\text{min}/60 \text{ sec})(1,000 \text{ g/kg})(\text{kg}/2.2 \text{ lb}) = 0.734 \text{ g/sec SO}_2$
- k: $(0.734 \text{ g/sec})(3,600 \text{ sec/hr})(\text{kg}/1,000 \text{ g})(2.2 \text{ lb/kg}) = 5.813 \text{ lb/hr SO}_2$
- l: $(0.0202 \text{ lb}/1,000 \text{ gal})(236,520,000 \text{ gal/yr})(\text{ton}/2,000 \text{ lb}) = 2.389 \text{ TPY SO}_2$

5.2 Emissions from the tank farm were based on the total combined gasoline throughput for Tank Nos. 1, 7, 9, 11, and 13 of 161,691,357 gallons per year. Emissions from the transmix tank were based on a gasoline throughput of 1,165,157 gallons per year. A 95% control efficiency was assumed for the vapor combustion system for processing vapors displaced from tank(s) storing transmix. A 10 mg CO emission per liter of gasoline loaded and 4 mg NO_x emission per liter of gasoline loaded were assumed based on information from Paragraph 5.1. It was also assumed that 0.202 lb SO₂ per liter of gasoline loaded was emitted from the vapor combustion system based on information from Paragraph 5.1. Vapor mass fractions of compounds for motor gasoline were multiplied by the total VOC emissions to determine total HAP emissions. Emissions for the review were only included from permitted tanks.

PROPOSED

Potential emissions from permitted tanks are shown in Enclosure (1) and summarized below.

Tank Farm Emissions								
Pollutant	TPY Emissions							
	Tank 1	Tank 2	Tank 7	Tank 9	Tank 11	Tank 13	Tank 14	Total
VOC	2.4	0.5	3.0	1.4	4.5	0.9	0.3	13.0
HAPs	0.051	0.011	0.064	0.030	0.095	0.019	0.006	0.276

5.3 Equipment leak emissions were determined based on New Equipment Leak Emission Factors for Petroleum Refineries, Gasoline Marketing, and Oil & Gas Production, February 1995 [EPA-453/R-95-017], Table 2.3. Emission factors were selected from the light liquid and gas groups for pumps, seals, valves, connectors, and other components. The number of pumps, valves, connectors, and other components were updated since the previous permit application. Vapor weight fractions of compounds from gasoline were multiplied by the total VOC emissions to determine HAP emissions. Emission estimates are shown in Enclosure (2) and summarized below as follows:

Equipment Leak Emissions						
Pollutant	Vapor Mass Fraction	Emission (TPY)				Total Emissions
		Fittings	Other	Pumps	Valves	
VOC	-----	0.336	0.114	0.104	0.388	0.9
Benzene	0.0060					0.006
Hexane (n)	0.0052					0.005
Toluene	0.0070					0.007
Xylene (-m)	0.0020					0.0021
Total HAPs----->						0.020

5.4 Worst-case yearly emissions of VOCs and HAPs from Kahului Marketing Terminal are as follows:

Facility Emissions				
Pollutant	Emissions (TPY)			Total Emissions (TPY)
	Bottom Loading Load Rack	Internal Floating Roof Tanks	Equipment Leaks	
VOCs	42.5	13.0	0.9	56.4
NO _x	4.0	-----	-----	4.0
CO	9.9	-----	-----	9.9
SO ₂	2.4	-----	-----	2.4
HAPS	0.880	0.276	0.020	1.176

6. Air Pollution Controls

- 6.1 The loading rack is equipped with a model no. ZCT-2-8-35-X2/8-X-X John Zink vapor combustion system to control VOC and HAP emissions. The maximum specified tank truck loading capacity for the vapor combustion system is 4,800 gallons per minute. Minimum specified tank truck loading rate for the vapor combustion system is 15 gallons per minute.
- 6.2 Tank Nos. 1, 2, 7, 9, 11, and 13 are equipped with internal floating roofs and tank seal systems to control VOC and HAP emissions.
- 6.3 Tank No. 14 may be equipped with a closed vent system and control device for controlling VOC and HAP emissions. If a control device is used for Tank No. 14 to reduce emissions, the control device will be the existing vapor combustion system servicing the load rack.

7. Air Quality Assessment

7.1 An ambient air quality impact assessment (AAQIA) was performed for the vapor combustion system because the applicant may use this control device to reduce TOC emissions according to 40 CFR Part 63, Subpart BBBBBB. Therefore, a slight increase in emissions will occur from extra vapors being directed to the control device from tank storage. Emissions from tank storage and the load rack were added to determine maximum pollutant impacts from the vapor combustion system. A SCREEN3 (Version 5) model was used for the analysis. Assumptions included:

- a. Flat terrain;
- b. Rural dispersion parameters;
- c. Default meteorology;
- d. Default receptors from 1 meter to 5,000 meters;
- e. Stack height, temperature, velocity, and diameter obtained from applicant's modeling assessment in permit application 0081-02;
- f. EPA scaling factors of 0.9, 0.7, and 0.4 for the 3-hour, 8-hour, and 24-hour concentrations, respectively; and
- g. State of Hawaii scaling factor of 0.2 for the annual concentration.

7.2 The following background concentrations were used for the AAQIA:

- a. NO_x (1-hr and annual) – collected in 2008 from the Kapolei air quality monitoring station (air monitoring station with NO_x data from another island closest to Kauai because there is no current background NO_x data from Kauai).
- b. CO (1-hr and 8-hr) – collected in 2008 from the Kapolei air quality monitoring station (air monitoring station with CO data from an island closest to Kauai because there is no current background CO data from Kauai).
- c. SO₂ (3-hr, 24-hr, and annual) – collected in 2008 from the Makaiwa air quality monitoring station (air monitoring station with SO₂ data from another island closest to Kauai because there is no current background SO₂ data from Kauai).

PROPOSED

7.3 The table below presents the emission rates and stack parameters used for the AAQIA.

Source	EMISSION RATE (g/s)			STACK PARAMETERS			
	NO _x	SO ₂	CO	Height	Temp.	Velocity	Dia.
Vapor Combustion System	1.220	0.734	3.038	35.1 ft	1,983 °F	40 ft/s	7.9 ft

7.4 Results in the table below show that the vapor combustion system complies with state and federal ambient air quality standards. The load rack was assumed to operate on a continuous basis at its maximum gasoline loading capacity (4,800 gallon per minute). Additional emissions due to processing vapors from transmix storage were assumed. Emissions from the transmix storage tank were based on a gasoline throughput of 1,165,157 gallons per year.

PREDICTED AMBIENT AIR QUALITY IMPACTS						
AIR POLLUTANT	AVERAGING TIME	IMPACT (ug/m ³)	BACKGROUND (ug/m ³)	TOTAL IMPACT (ug/m ³)	AIR STANDARD (ug/m ³)	PERCENT STANDARD
SO ₂	3 – Hour	2.1	47	49.1	1,300	4
	24 – Hour	0.9	20.9	21.8	365	6
	Annual	0.5	2.6	3.1	80	4
NO ₂	Annual	0.8	7.5	8.3	70	12
	1 – Hour	3.9	56.4	60.3	188	32
CO	1 – Hour	9.6	2,519	2,528.6	10,000	25
	8 – Hour	6.7	801.5	808.2	5,000	16

8. Significant Permit Conditions

8.1 Add conditions that incorporate control measures for equipment leaks, tanks, and the loading rack's vapor processing system pursuant to 40 CFR Part 63, Subpart BBBBBB.

Reason for 8.1: 40 CFR Part 63, Subpart BBBBBB was promulgated on January 10, 2008. Chevron Products Company must comply with the federal standard no later than January 10, 2011.

9. Conclusions and Recommendation

9.1 Actual emissions from the facility should be less than those estimated because the terminal does not operate on a continuous basis. The terminal is equipped with a vapor combustion system to control VOC and HAP emissions from tank truck loading operations and the transmix tank that may store gasoline as worst-case. The internal floating roofs and tank seal systems for Tank Nos. 1, 2, 7, 9, 11, and 13 provide additional control of VOC and HAP emissions. Recommend issuance of the permit subject to incorporation of the significant permit conditions. The 30-day public comment period and 45-day EPA review period will be initiated simultaneously.

Mike Madsen 8-5-2010